AMENDMENTS TO THE CLAIMS

1. (Previously Presented) A process to prepare a heavy base oil having a kinematic viscosity at 100 °C of above 15 cSt and a light lubricating base oil having a kinematic viscosity at 100 °C of between 3.8 and 6 cSt from a partly isomerized Fischer-Tropsch derived feedstock, said feedstock having an initial boiling point of below 400 °C and a final boiling point of above 600 °C and the fraction boiling above 540 °C is at least 20 wt%, said process comprising:

(a) separating, via distillation , said fraction into a light base oil precursor fraction and a heavy base oil precursor fraction;

(b) reducing the pour point of each separate base oil precursor fraction by means of dewaxing; and,

(c) and isolating the desired base oil products from said dewaxed oil fractions as obtained in step (b).

2. (Previously Presented) The process of claim 1, wherein the effective cut temperature in step (a) at which the light and heavy base oil precursor fractions are separated is between 470 °C and 600 °C.

3. (Previously Presented) The process of claim 1, wherein the fraction boiling above 540 °C in the feed to step (a) is at least 30 wt%.

4. (Previously Presented) The process of claim 1, wherein the heavy base oil as obtained in step (c) has a kinematic viscosity at 100 °C of above 17 cSt.

5. (Previously Presented) The process of claim 4, wherein a base oil having a kinematic viscosity at 100 °C of between 7 cSt and 15 cSt is isolated from the dewaxed light base oil precursor fraction.

6. (Previously Presented) The process of claim 1, wherein the dewaxing of the heavy and light base oil precursor fraction is performed simultaneously in two different reactors.

7. (Previously Presented) The process of claim 1, wherein the dewaxing step is performed by means of a catalytic dewaxing process in the presence of a catalyst comprising a medium pore size molecular sieve and a Group VIII metal.

8. (Previously Presented) The process of claim 7, wherein the molecular sieve is selected from the group consisting of a MTW, MTT and TON type molecular sieve.

9. (Previously Presented) The process of claim 7, wherein the Group VIII metal is platinum or palladium.

10. (Previously Presented) The process of claim 7, wherein the catalyst used in the catalytic dewaxing of the heavy base oil precursor fraction comprises a MTW molecular sieve, platinum or palladium as Group VIII metal and a silica binder.

11. (Previously Presented) The process of claim 10, wherein the catalytic dewaxing of both light and heavy base oil precursor fractions is performed in the presence of a catalyst comprising a MTW molecular sieve, platinum or palladium as Group VIII metal and a silica binder.

12. (Previously Presented) The process of claim 1, wherein the heavy base oil precursor fraction is reduced in pour point by first performing a pour point reducing step in the presence of a catalyst comprising a 12-member ring zeolite and secondly performing a catalytic dewaxing on the effluent of the first step in the presence of a 10-member ring zeolite.

13. (Previously Presented) The process of claim 12, wherein the pour point after the first dewaxing step is between -10 °C and +10 °C.

14. (Previously Presented) The process of claim 2, wherein the fraction boiling above 540 °C in the feed to step (a) is at least 30 wt%.

15. (Previously Presented) The process of claim 1, wherein the heavy base oil as obtained in step (c) has a kinematic viscosity at 100 °C of above 20 cSt.

16. (Previously Presented) The process of claim 15, wherein a base oil having a kinematic viscosity at 100 °C of between 7 cSt and 15 cSt is isolated from the dewaxed light base oil precursor fraction.

17. (Previously Presented) The process of claim 8, wherein the Group VIII metal is platinum or palladium.

18. (Previously Presented) The process of claim 2, wherein the heavy base oil precursor fraction is reduced in pour point by first performing a pour point reducing step in the presence of a catalyst comprising a 12-member ring zeolite and secondly performing a catalytic dewaxing on the effluent of the first step in the presence of a 10-member ring zeolite.

19. (Previously Presented) The process of claim 18, wherein the pour point after the first dewaxing step is between -10 °C and +10 °C.

20. (Currently Amended) The process of claim 3, wherein the heavy base oil as obtained in step (c) ~~as~~ has a kinatic viscosity[[t]] at 100 °C of above 20 cSt.